## Study on a New Method of Extraction of Metal Ions from Solid Matrices by Supercritical Fluid

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**Abstract:** 8-Hydroxyquinoline, methanol and Triton-100 were first used together in the extraction of metal ions by supercritical CO<sub>2</sub>. In the new system, the effects of pressure, temperature and the volume of CO<sub>2</sub> on the efficiency of supercritical fluid extraction (SFE) were systematically investigated. The recovery under the optimum condition was only 11.38%, but if suitable concentration of methanol (v/v=5%) was added to the supercritical CO<sub>2</sub>, the recovery was increased significantly (83.60%, RSD=4.37%, n=5). In order to further enhance the recovery Triton X-100 was added to the samples, and the results were satisfactory (96.62%, RSD=2.85%, n=5).

Keywords: Supercritical fluid extraction, chelating agent, modifier, surfactant, metal ions, solid matrices.

To date, most of the published SFE works have focused on organic compound<sup>1</sup>, and some reports have related to SFE of metal ions<sup>2</sup>. Direct extraction of metal ions by supercritical CO<sub>2</sub> is highly inefficient. One approach of extracting metal ions by supercritical CO<sub>2</sub> is suggested to convert the charged metal ions into neutral metal complexes by using chelating agent in the supercritical CO<sub>2</sub>. A variety of organic chelating agents such as thiocarbamate,  $\beta$ -diketones, and crown ether have been used in SFE of metal ions<sup>3</sup>.8-Hydroxyquinoline contains double coordination atoms (**N**, **O**<sup>-</sup>), so it is easy to react with Cu<sup>2+</sup> and form stable neutral chelate. 8-Hydroxyquinoline was used as chelating agent in the complexation-SFE of Cu<sup>2+</sup>, and we obtained satisfying results.

### **Experimental**

Supercritical fluid extractor (made in Shandong University and Lunan Chemical Instrumental Plant), 754 model ultraviolet and visible spectrophotometer (made in the Third Analytical Instrumental Plant of Shanghai).

In order to find the optimum condition of the extraction of  $Cu^{2+}$ , different pressures, temperatures, the volumes of  $CO_2$  have been studied. Under the optimum condition found above, the supercritical  $CO_2$  containing 5% (v/v) methanol was used in the extraction. Then aliquot of microemulsion containing Triton X-100 was added to the samples. Finally, the metal chelates were collected in 10 ml chloroform and were determined by ultraviolet and visible spectrophotometer.

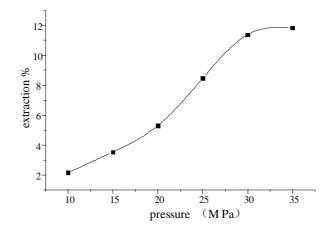
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#### **Results and Discussion**

## Effect of pressure on the recovery of $Cu^{2+}$

The efficiency of extracting  $Cu^{2+}$  at 60°C with different pressure of  $CO_2$  was shown in **Figure 1**. As the other condition is constant, with the increase of the pressure of  $CO_2$  the density of  $CO_2$  increases, and the solvent strength of supercritical  $CO_2$  increases correspondingly, this lead to the increase of the solubility of Cu (8-Hydroxyquinoline)<sub>2</sub> in supercritical  $CO_2$ , it is beneficial to the extraction. When the pressure of  $CO_2$  increases, the ability of supercritical  $CO_2$  to transport Cu (8-Hydroxyquinoline)<sub>2</sub> from active sites on the surface of the matrices into the fluid phase decreases, and the losses of analytes increase due to both volatilization and the formation of aerosols. These are not beneficial to the extraction. So there are three functions in the process of extraction and they compete with each other. In the range of 10 MPa – 30 MPa, the first function is prominent. So the efficiency of extraction increases constantly, therefore the efficiency of extraction increases increase the efficiency of extraction increases increase the efficiency of extraction increases increase the efficiency of extraction increases increases the efficiency of extraction increases increase the efficiency of extraction increases increases the efficiency of extraction increases increases increases were slowly.

**Figure 1**. Effect of the pressure on the recovery of  $Cu^{2+}$  at 60°C (The time of static extraction :20min, The volume of supercritical CO<sub>2</sub> used in dynamic extraction :10 ml)



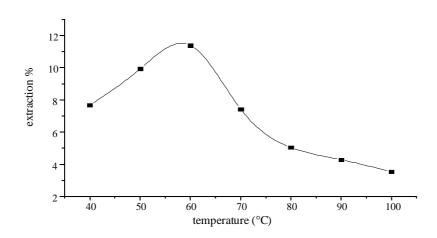
Effect of temperature on the extraction of  $Cu^{2+}$ 

The effect of temperature on the efficiency of extraction of  $Cu^{2+}$  is shown in **Figure 2**. As the other condition is constant, based on the rule of kinetics, the higher the temperature the more intensive the heat motion of solutes on the active sites of the matrices. It is beneficial for the solutes to overcome the adsorbing energy fortress of the matrices and to escape from the surface of the matrices into the supercritical CO<sub>2</sub>. In the point of view of thermodynamics, when the temperature increases the saturation vapor-pressure increases correspondingly, this makes the solutes to dissolve in the supercritical CO<sub>2</sub> easily. When the temperature increases the density of supercritical carbon dioxide

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decreases, which makes the solvent strength of supercritical carbon dioxide decrease correspondingly, therefore the solubility of metal chelates in supercritical carbon dioxide decreases. The three factors compete with each other. Figure 2 shows that the largest efficiency of extraction was obtained at  $60^{\circ}$ C. So  $60^{\circ}$ C was selected as optimum temperature.

**Figure 2.**Effect of temperature on the recovery of Cu<sup>2+</sup> at 30 MPa (The time of static extraction: 20 min, the volume of supercritical CO<sub>2</sub> used in dynamic extraction: 10 ml, the flow rate of supercritical CO<sub>2</sub>: 1 ml/min)



Effect of volume of the supercritical  $CO_2$  on the recovery of  $Cu^{2+}$ 

When the volume of supercritical  $CO_2$  used in the extraction increases, the balance of extraction is beneficial to move to the direction of extraction of Cu (8-Hydroxyquinoline)<sub>2</sub>. But with the volume of  $CO_2$  increases the supercritical  $CO_2$  emited from restrictor increases, this leads to the increase of the losses of analytes due to both volatilization and the formation of aerosols, it is not beneficial to increase the recovery. The flow rate of  $CO_2$  was fixed at 1 ml/min, 10 ml, 15 ml, 20 ml, 25 ml, 30 ml, 35 ml, 40 ml are selected as the volumes of  $CO_2$  respectively, the result showed that in the range of 10 ml-35 ml the efficiency increases increases and in the range of 35 ml-40 ml the efficiency decreases slowly. So 35 ml was selected as the optimum volume of  $CO_2$ .

## *Effect of the modifier on the recovery of* $Cu^{2+}$

Improved solvent characteristics and extraction efficiencies can be obtained if polar solvent such as methanol is added to the supercritical  $CO_2$ . Polar modifier is thought to aid extraction in two ways: increasing the solvent strength of the supercritical fluid as well as interacting with the analyte/matrices complex to promote rapid desorption into the supercritical  $CO_2$ . As we know  $CO_2$  is nonpolar but Cu (8-Hydroxyquinoline)<sub>2</sub> is polar metal complex. Suitable amounts of modifier can enhance the polarity of supercritical  $CO_2$ . This increases the interaction between polar solutes and modified solvent. Methanol was chosen in our experiment because of its high solvent polarity parameter, and its ability to deactivate the active sites on the surface of solid matrices.

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The results of extraction of  $Cu^{2+}$  using a commercially available SFC grade  $CO_2$  containing 5% (v/v)methanol are summarized in **Table 1**. The methanol-modified  $CO_2$  increases the extraction efficiency of  $Cu^{2+}$  from 11.38 % to 83.60 %.

**Table 1.** Effect of the modifier on the recovery of  $Cu^{2+}$  at 60°C, 30 MPa (The time of static extraction: 20 min, the volume supercritical CO<sub>2</sub> used in dynamic extraction : 35 ml, the flow rate of supercritical CO<sub>2</sub>: 1 ml/min)

| Number | Modifier     | Efficiency of extraction (%) |  |
|--------|--------------|------------------------------|--|
| 1      | Methanol(5%) | 80.39                        |  |
| 2      | Methanol(5%) | 85.78                        |  |
| 3      | Methanol(5%) | 83.28                        |  |
| 4      | Methanol(5%) | 87.54                        |  |
| 5      | Methanol(5%) | 81.02                        |  |

RSD=4.37%, n=5, Average value = 83.60%.

Effect of the surfactant on the recovery of  $Cu^{2+}$ 

The efficiency of extracting  $Cu^{2+}$  by supercritical  $CO_2$  modified by methanol was further improved in the presence of a non-ionic surfactant Triton X-100. The efficiency of extracting  $Cu^{2+}$  achieved 96.62%. Triton X-100 serves the function of solubilization. It is beneficial to the dissolution of the Cu (8-Hydroxyquinoline)<sub>2</sub> in the supercritical CO<sub>2</sub> and desorption of Cu (8-Hydroxyquinoline) <sub>2</sub> from the active sites of the matrices to the supercritical CO<sub>2</sub>. The result are shown in **Table 2**.

**Table 2.** Effect of the surfactant on recovery of  $Cu^{2+}$  at 60°C, 30MPa(The time of static extraction: 20 min, the volume of supercritical CO<sub>2</sub> used in dynamic extraction : 35 ml, the flow rate of supercritical CO<sub>2</sub>: 1 ml/min)

| Number | Modifier     | Surfactant  | Efficiency of extraction (%) |
|--------|--------------|-------------|------------------------------|
| 1      | Methanol(5%) | TritonX-100 | 93.09                        |
| 2      | Methanol(5%) | TritonX-100 | 95.34                        |
| 3      | Methanol(5%) | TritonX-100 | 100.01                       |
| 4      | Methanol(5%) | TritonX-100 | 96.38                        |
| 5      | Methanol(5%) | TritonX-100 | 98.26                        |

RSD=2.85%, n=5, Average value = 96.62%.

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